

# 16.901: Optimization Project

## Design of Film Cooling for Combustor Liners

### Sample Solution

## 1 Background

The temperatures within the primary zone of a combustor are significantly higher than the temperatures which most materials can withstand without significant deterioration. Thus, a critical aspect of the design of a combustor is the development of a method to cool the liner walls of a combustor such that the temperatures which the liner temperatures are well below the limit of the material. A typical method to cool a combustor liner is through film cooling. Film cooling consists of diverting air from the main flow path prior to combustion and then re-introducing this air along the liner surface to provide a film of cooler air to protect the liner.

In this project, you will consider the optimization of a liner film cooling design. The numerical simulation of the liner cooling is based on the finite-difference method developed in Project Two for 16.901. In this project, the cooling air velocity,  $U_{cool}$ , and the height of the cooling film,  $h$ , are the two design variables. To make certain that the design is realistic, the design variables are bounded by:

$$\begin{aligned} 50 \text{ m/s} &\leq U_{cool} \leq 250 \text{ m/s} \\ 0.001 \text{ m} &\leq h \leq 0.005 \text{ m} \end{aligned}$$

The values (or range of values) of all the parameters are given in Table 1.

Parameter	Definition	Value
$k_g$	air conductivity	0.1 W/(m K)
$k_w$	wall conductivity	26.0 W/(m K)
$h$	height of cooling passage	0.001 - 0.005 m
$L$	axial length between cooling passages	0.3 m
$U_{hot}$	velocity of hot flow	100 m/sec
$U_{cool}$	velocity of cool flow	50 - 250 m/sec
$T_{hot}$	temperature of hot flow	2200 K
$T_{cool}$	temperature of cool flow	800 K
$t_w$	thickness of liner wall	0.0015 m

Table 1: Parameter definitions and values

## 2 Tasks

### 2.1 Minimization of liner temperature (20%)

In this first task, we consider the minimization of the maximum liner temperature,  $T_{max}$ . Note,  $T_{max}$  is assumed to occur on the upper surface at the outlet of the computational domain. The design parameters were non-dimensionalized and mapped such that they both range from  $-1$  to  $+1$  as follows:

$$x_1 = -1 + 2 \frac{U_{cool} - \min U_{cool}}{\max U_{cool} - \min U_{cool}} \quad x_2 = -1 + 2 \frac{h - \min h}{\max h - \min h}$$

where  $\min U_{cool}$  is the lower bound of the design range for  $U_{cool}$ , etc. Then, Matlab's **fmincon** optimization routine was used to minimize  $T_{max}$  over the design space. **fmincon** calculated the necessary derivatives through finite differencing for this task. The minimal value was found to be  $T_{max} = 1180.4 \text{ K}$  and occurred at  $U_{cool} = 250 \text{ m/sec}$  and  $h = 0.005 \text{ m}$ . This design point is logical since the minimum temperature is expected to occur for

the design with the maximum cooling air flow and height. Clearly,  $U_{cool}$  and  $h$  are at the boundary of the design space.

The optimization for this problem was begun at the center of the design space (i.e. at  $U_{cool} = 150$  m/sec and  $h = 0.003$  m). The optimization history was

UseIter	F-count	f(x)	constraint	Step-size	derivative	Procedure
1	3	-0.0099065	-1	1	-0.037	
2	7	-0.0235035	-0.8135	1	-1.66e+05	Hessian modified
3	11	-0.0920041	0	1	-1.8e-09	

Optimization terminated successfully:

Search direction less than 2\*options.TolX and

maximum constraint violation is less than options.TolCon

Active Constraints:

3

4

The main Matlab source code for the temperature minimization is the **minT.m** script.

## 2.2 Minimization of cooling mass flow (20%)

In this task, we minimize the mass flow in the cooling film for a given maximum temperature limit. Specifically, we solve the following problem:

$$\min \dot{m} = U_{cool}h \text{ such that } T_{\max} = T_{lim}.$$

In this task,  $T_{lim} = 1300$  K. The temperature constraint is set in the following non-dimensional manner:

$$\frac{T_{\max}}{T_{lim}} - 1 = 0.$$

As in the previous case, finite-difference derivatives have been used. The main script for the optimization is in **optliner.m**. Starting from the center of the design space, the optimal design occurs for  $U_{cool} = 189.7$  m/sec and  $h = 0.001$ m, giving a mass flow of  $\dot{m} = 0.192$  m<sup>2</sup>/sec. The iteration history for the case is:

Iter	F-count	f(x)	max constraint	Step-size	Directional derivative	Procedure
1	3	0.45	0.009906	1	-0.0656	
2	7	0.384226	0.006096	1	0.097	Hessian modified twice
3	25	0.38422	0.006096	-6.1e-05	-0.0227	
4	29	0.360757	0.002662	1	0.00674	
5	33	0.367434	0.0001362	1	0.000366	Hessian modified
6	37	0.367799	7.998e-06	1	-0.000152	Hessian modified twice
7	41	0.367647	2.128e-06	1	-0.0102	Hessian modified twice
8	45	0.35741	7.668e-05	1	-0.0181	
9	49	0.338858	0.0003395	1	-0.17	Hessian modified twice
10	53	0.154972	0.02271	1	0.0173	
11	57	0.172227	0.01157	1	0.00926	
12	61	0.181486	0.006055	1	0.00995	
13	65	0.191484	0.0006509	1	0.00118	
14	69	0.192632	8.006e-05	1	-0.000587	Hessian modified twice
15	73	0.191928	0.0001628	1	0.0003	Hessian modified
16	77	0.192227	1.209e-06	1	-1.23e-05	Hessian modified

Optimization terminated successfully:

### 2.3 Minimization of cooling mass flow with analytic derivatives (40%)

Analytic sensitivity derivatives were added to the Matlab source code for the objective function (i.e.  $\dot{m}$ ) and the constraint equation with respect to the design variables. The derivatives of  $\dot{m}$  are simple as they depend directly on the design variables,

$$\begin{aligned}\frac{d\dot{m}}{dU_{cool}} &= h, \\ \frac{d\dot{m}}{dh} &= U_{cool}.\end{aligned}$$

Since the design variables have been non-dimensionalized, the sensitivity derivatives with respect to the scaled design variables are,

$$\begin{aligned}\frac{d\dot{m}}{dx_1} &= \frac{\max U_{cool} - \min U_{cool}}{2} \frac{d\dot{m}}{dU_{cool}}, \\ \frac{d\dot{m}}{dx_2} &= \frac{\max h - \min h}{2} \frac{d\dot{m}}{dh}.\end{aligned}$$

The constraint equation depends on the states of the finite-difference film-cooling model. Specifically, the value of  $T_{\max}$  is the temperature at on the upper surface at the outlet which is found by solving the finite-difference model. For example, consider the dependence of  $T_{\max}$  on  $h$ , the derivative may be found as follows,

$$\frac{dT_{\max}}{dh} = \frac{\partial T_{\max}}{\partial h} + \frac{\partial T_{\max}}{\partial \vec{T}} \frac{d\vec{T}}{dh}, \quad (1)$$

where  $\vec{T}$  is the vector of temperatures solved in the finite-difference model. Since  $T_{\max}$  does not directly depend on the design variables,  $\frac{\partial T_{\max}}{\partial h} = 0$ . Furthermore,  $\frac{\partial T_{\max}}{\partial \vec{T}}$  is a vector of zeros except for the entry corresponding to the upper surface, outlet location where the derivative is one. Thus, the remaining difficulty is to find  $\frac{d\vec{T}}{dh}$ . Writing the governing equations of the finite-difference model as a set of residual equations we have,

$$\vec{R}(\vec{T}, h) = 0.$$

Note, the residual equation also depends on  $U_{cool}$  but for this derivation, we have not shown this explicitly. Then, if we consider a perturbation in  $h$  which will create a perturbation in  $\vec{T}$ , we have,

$$\vec{R}(\vec{T} + d\vec{T}, h + dh) = 0.$$

Then, in the limit of small changes, we may Taylor series this result to produce,

$$\vec{R}(\vec{T} + d\vec{T}, h + dh) \approx \vec{R}(\vec{T}, h) + \frac{\partial \vec{R}}{\partial \vec{T}} d\vec{T} + \frac{\partial \vec{R}}{\partial h} dh = 0.$$

Or, re-arranging this we find,

$$\frac{\partial \vec{R}}{\partial \vec{T}} \frac{d\vec{T}}{dh} = -\frac{\partial \vec{R}}{\partial h}.$$

Plugging this result into Equation (1) gives,

$$\frac{dT_{\max}}{dh} = -\psi^T \frac{\partial \vec{R}}{\partial h},$$

where the adjoint  $\psi$  satisfies,

$$\frac{\partial \vec{R}}{\partial \vec{T}}^T \psi = \frac{\partial T_{\max}}{\partial \vec{T}}^T.$$

A similar result exists for  $U_{cool}$ ,

$$\frac{dT_{\max}}{dU_{cool}} = -\psi^T \frac{\partial \vec{R}}{\partial U_{cool}}.$$

This adjoint-based sensitivity derivative was implemented in **condif.m**.

For the constraint  $T_{lim} = 1300 K$ , the optimization was re-run with the analytic derivatives. The optimum occurs for  $U_{cool} = 190.5$  m/sec and  $h = 0.001$ m, giving a mass flow of  $\dot{m} = 0.192$   $m^2/sec$  and clearly matches the finite-differenced derivative optimization from Section 2.2. The iteration history for the case is:

Iter	F-count	f(x)	max constraint	Step-size	Directional derivative	Procedure
1	1	0.45	0.009906	1	-0.0943	
2	3	0.359221	0.0001474	1	-0.173	
3	6	0.266075	7.981e-06	0.5	-0.0976	Hessian modified twice
4	9	0.215392	0.001534	0.5	-0.0394	
5	12	0.194336	0.002947	0.5	-0.0073	
6	14	0.183999	0.004592	1	0.00811	
7	16	0.192196	0.0001133	1	8.32e-06	Hessian modified
8	18	0.192168	4.955e-05	1	1.9e-05	Hessian modified
9	20	0.192162	3.339e-05	1	6.11e-05	Hessian modified
10	22	0.192224	3.274e-08	1	6e-08	Hessian modified

Optimization terminated successfully:

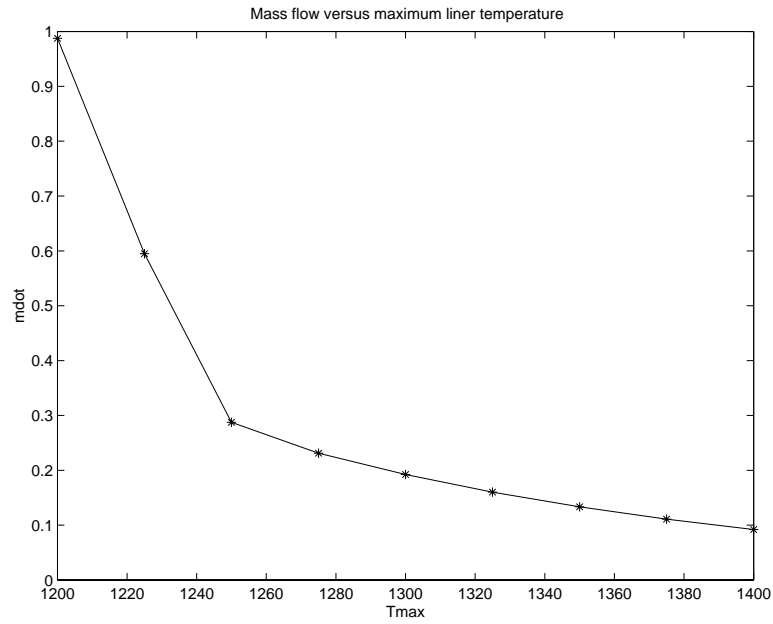
Comparing the work with finite-difference sensitivity derivatives to the adjoint-based analytic derivatives, clearly the finite-differenced sensitivity derivative case required 77 function evaluations compared to only 22 evaluations for the analytic derivatives. We note, however, that the analytic derivatives requires the inversion of  $\frac{\partial \vec{R}}{\partial \vec{T}}$ . Thus, a single evaluation of the function and derivatives is about twice as expensive than a single function evaluation in the finite-differenced version.

## 2.4 Parametric study of cooling mass flow minimization (20%)

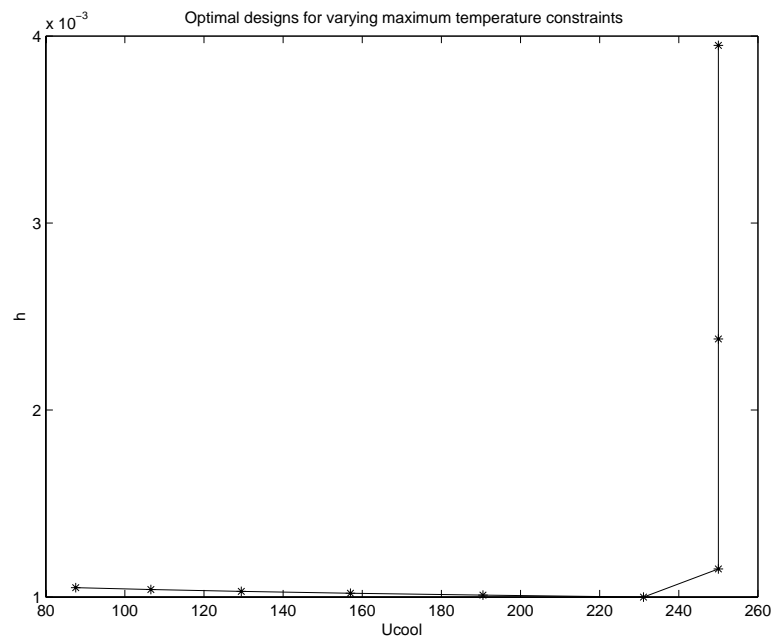
Using the constrained optimization with analytic derivatives developed in the previous section, a trade study was performed by varying  $T_{lim}$  from 1200 K to 1400 K. The results are shown in Figure 1.

The variation of  $\min \dot{m}$  versus  $T_{lim}$  shows that  $\dot{m}$  increases with decreasing  $T_{lim}$ . This trend is expected as the lower temperature will require larger liner cooling, and therefore higher mass flows.

The location of the designs in the two-dimensional design space show that at the most stringent temperature constraint (i.e. lowest  $T_{lim}$ ), the largest mass flow is used with  $U_{cool}$  at its maximum value and  $h$  nearly at its largest value. As  $T_{lim}$  is increased, the  $h$  value decreases while  $U_{cool}$  remains at the maximum limit of 250 m/sec. Eventually, at  $T_{lim} = 1275K$ , the value of  $U_{cool}$  decreases from the maximum boundary value. At this point, further increases in  $T_{lim}$  cause further decreases of  $U_{cool}$  while  $h$  is fixed at the minimum value of 0.001 m.



(a) Optimum  $\dot{m}$  versus  $T_{lim}$



(b) Optimum design variables versus  $T_{lim}$

Figure 1: Trade study for varying maximum temperature limits,  $T_{lim}$ .